A Facile Approach to the CSR Determination of Metallurgical Coke

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ABSTRACT: One of the key parameters in the assessment of metallurgical coke quality is Coke Strength after Reaction (CSR) and the concomitant Coke Reactivity Index (CRI). The standard for these two parameters requires industrial metallurgical coke for the measurement. In practice, CanmetENERGY uses metallurgical coke obtained from one or other of its pilot-scale coke ovens (460 mm wide, 350 kg capacity) which produce the required industrial-grade coke. The only option for determining the CSR of a particular met coal or blend is to perform a pilot-scale test to produce the appropriate coke for the measurement. When the full amount of coal for pilot oven testing is not available, as might be the case for a sample of limited quantity such as from an exploration bore hole, CSR cannot normally be measured.

In an effort to broaden the scope of CSR measurement, CanmetENERGY has developed a novel procedure for its determination using significantly smaller amounts of coal sample (~12-13 kg) making use of the Sole-Heated Oven in accordance with ASTM D2014-97(2010) Standard. Preparing the coke sample in the sole-heated oven produces a semi-coke that has been heated from the bottom side to 950 °C and the top side to 500 °C over a period of 6-7 hrs. This semi-coke is quenched with water and subsequently heat-treated at 1100 °C for one hour under nitrogen. CSR is then determined on the resulting coke according to ASTM D5341-99(2010) Standard. To validate this approach, CSR's were also determined on identical blends concurrently using CanmetENERGY's pilot scale movable wall test oven.

An analysis of the results indicates the significance of the smaller-scale CSR measurements and their relevance to industrial-scale coke characterization. Coke textural analysis for the cokes validates this novel approach for determination of CSR.

Keywords: Coke, Cokemaking, CSR, CRI, Carbon Forms

Introduction

Current world-wide ironmaking capacity is dominated by blast furnace technology. In 2009, this technology accounted for 94% of global hot metal production, 912.2 Mt[1]. In comparison, direct reduced iron (DRI) production was limited to only 53.1 Mt[2]. The performance and efficiency of blast furnace ironmaking technology is continuously improving. One of the factors contributing to the success of blast furnace ironmaking is the continued amelioration in coke quality.

Metallurgical coke is the major source of carbon in the operation of the blast furnace. Besides being responsible for producing reducing gas, coke also supports the descending burden and provides passages/voids through it for distributing reducing gas in the furnace. Moreover, the combustion of coke in the lower hearth by the injected blast generates heat for melting of the hot metal. Because of the numerous functions of coke in the blast furnace, stringent requirement on its physical and chemical properties are needed to ensure smooth operation of high productivity modern blast furnaces[3].

In the lower hearth of the blast furnace, coke is the only solid material present to support the entire weight of the burden above. Coke, possessing high mechanical strength in extremely hot and dynamic environments, is required to cope with the increase in throughput of large sized blast furnaces. Prior to its descent to the lower hearth, coke reacts with CO_2 produced from the reduction of iron ore to generate CO to replenish the source of this reducing gas required for reduction of iron ore in the upper portion of the furnace. Therefore, the coke charged into the blast furnace must be capable of generating CO by reacting with CO_2 while simultaneously maintaining its physical strength after reaction.

Among the important indicators for assessing the quality of coke for blast furnace application are Coke Reactivity Index (CRI) and Coke Strength after Reaction (CSR) developed by Nippon Steel Corporation in the early 1970s[4].

To estimate the quality of coke produced from specific coal blends in terms of CSR and CRI, the most economical way is by carrying out carbonization in a pilot-scale coke oven having known and proven capability of producing industrial grade coke.

CanmetENERGY currently operates two pilot-scale slot-type coke ovens (460 mm wide and 350 kg capacity). The pilot-scale coke oven used in this investigation is depicted in Figure 1.

Figure 1. CanmetENERGY Pilot-Scale Coke Oven

The cokes produced in either of these ovens have been shown over time to be of similar quality to industrial coke via benchmarking against industrial ovens[5].

The pilot scale oven test requires a specific amount of coal to ensure the coke produced is appropriate for CSR evaluation. In such instances where the amount of coal available is insufficient to perform a pilot-scale test, as for the case of an exploration bore hole sample, CSR and CRI normally cannot be measured.

In an effort to broaden the ability to measure CSR and CRI with limited amounts of coal sample, a novel procedure for producing coke involving carbonization using a sole-heated oven was developed at CanmetENERGY. The sole-heated used in this study is shown in Figure 2.

Figure 2. CanmetENERGY Sole-Heated Oven

To validate this new approach for producing coke for CSR and CRI evaluation, concurrent carbonization tests of identical coal blends using sole-heated oven and pilot-scale moveable wall oven were performed. CSR and CRI of the cokes produced using both carbonization routes were compared.

Besides comparing sole-heated oven and pilot-scale oven cokes for their CSR and CRI, these were also evaluated for their Apparent Specific Gravity (ASG), the ratio of the mass of a volume of dry coke to the mass of an equal volume of water. Coke ASG varies with the rank and ash content of the coal carbonized, the bulk density of the coal charge in the oven, the carbonization temperature and the coking time[6].

Furthermore, microscopical analysis of the textures was performed on the sole-heated and pilot-scale oven cokes to compare them for their carbon forms. As discussed later, this technique is, among numerous advantages, extremely useful for understanding the behaviour of coal during coking and for interpreting pilot movable wall oven results including pressure generation and coke quality results.

Experimental

1. Coke Preparation in Sole-Heated Oven for CSR/CRI Determination

The preparation of a coke sample for CSR evaluation using a coal sample of limited quantity involves two steps:

(1) Semi-Coke Preparation

(2) Heat Treatment

For preparation of semi-coke, the sole-heated oven was employed in accordance with the ASTM D2014-97(2010) Standard for expansion or contraction of coal.

A total of 12 kg of sample (coal or blends) is divided equally and each half-charged into chambers approximately 280 mm in width, length and depth of a double-chambered oven. A weighted piston applies a constant load of 15.17 ± 0.35 kPa on the surface of the coal in each of the chambers throughout the test. The coal bed is heated from below by the sole plate initially set at 554 °C and gradually ramped up to 950 °C according to a prescribed temperature program. The test is considered complete when the temperature at the top of the coal bed reaches 500 °C after a period of 6-7 hours. Following completion of the test, the coke is pushed from the oven, quenched in water, drained and oven dried overnight at 120 °C. In cases where expansion/contraction values are reported, the measured expansion or contraction of the sample is converted to a reference base of 833 kg/m^3 and 2% moisture.

For heat treatment, the dried semi-coke (8-9 kg) is subsequently introduced in pieces (50 x 175 mm) into a stainless steel holding box hermetically sealed on top with 3 mm thick section of stainless steel with a 1 cm exit hole in the centre for venting the hot coke gases. The holding box is connected to N_2 gas for continually flushing the semi-coke (5-10 L/min flowrate) to prevent its combustion. The holding box with the semi-coke inside is then heated in a Muffle Furnace from ambient to 1100 °C in 2-3 h at the rate of 5-10 °C/min. Upon attaining 1100 °C, the coke is soaked for an additional hour. Then, cooling is allowed to take place to approximately 100 °C. The entire heating and cooling cycle is carried out in a continuous flow of N_2 and requires about15 hrs to complete. The average weight loss of coke during the heat-treatment process has been measured to be 5 ± 2%.

After the heat treatment, the coke sample produced was prepared and tested for CSR and CRI measurement as per specifications in the ASTM D5341-99(2010) Standard. By definition, the CRI is the percent weight loss of the coke sample after reaction in CO_2 at 1100°C for 2 hours. The cooled, reacted coke is then tumbled in an I-drum for 600 revolutions at 20 rpm. The cumulative percent of +9.5 mm coke after tumbling is denoted as the CSR. The repeatability limit (r) of this method for CRI is 2.4 and for CSR is 5.4; the reproducibility limit (R) of this method for cokes in CRI range 20-28 is between 5 and 7 and that for cokes in CSR range 55-70 (acceptable grade for ironmaking) is also between 5 and 7.

2. Coke Apparent Specific Gravity (ASG) Determination

ASG of cokes were determined following a method developed at CanmetENERGY and related to the ASTM D167-93(2004) and ISO 1014:1985 Standards.

3. Carbon Form Analysis

Carbon form analysis in this study was carried out as per a combination of the US Steel method[7] and the CanmetENERGY method. A single point count is made for each measured field of view. For each field, the stage is rotated in order to determine the possible highest rank carbon form. Table 1 contains a tabular summary of an example result using this method. Normally 500 point counts are performed on a sample. Each carbon form is derived from an assumed parent coal V-type. From the coke texture analysis, one can determine the 'effective coal reflectance (%Ro)' and also the percentages of low-, medium- and high-volatile parent coals used in the blend.

The CMSI[8] is the coke mosaic size index defined as:

$$\text{CMSI} = \frac{\{(\%\text{Incipient}) + 2(\%\text{CF} + \%\text{CM}) + 3(\%\text{CC} + \%\text{LF} + \%\text{LM}) + 4(\%\text{LC} + \%\text{RF}) + 5(\%\text{RM} + \%\text{RC})\}}{(100 - \%\text{Isotropic} - \%\text{Total Inerts})}$$

This is a mathematical method to summarize the carbon form analysis. The formula used in this work is an adaptation of Coin's method. The higher the CMSI, the higher the rank based on carbon forms measured.

Table 1. Carbon Form Analysis Example

SAMPLE DESCRIPTION	Example							
TEXTURE	FREQUENCY COUNTS	BINDER PHASE	BINDER,FILLER AND MISC	PARENT COAL RO	COKE YIELD	COKE TO COAL	COAL WEIGHT	RO CALC
ISOTROPIC	13	3.49	2.58	0.70	61.21	4.21	4.07	2.85
TOTAL ISOTROPIC	**13**	**3.49**	**2.58**					
INCIPIENT	23	6.18	4.56	0.85	64.70	7.05	6.81	5.79
CIRCULAR FINE	145	38.98	28.77	0.95	67.03	42.92	41.44	39.37
CIRCULAR MEDIUM	3	0.81	0.60	1.05	69.35	0.86	0.83	0.87
CIRCULAR COARSE	0	0.00	0.00	1.15	71.68	0.00	0.00	0.00
TOTAL CIRCULAR	**171**	**45.97**	**33.93**	.	.	.	.	.
LENTICULAR FINE	64	17.20	12.70	1.25	73.79	17.21	16.61	20.77
LENTICULAR MEDIUM	32	8.60	6.35	1.35	75.58	8.40	8.11	10.95
LENTICULAR COARSE	8	2.15	1.59	1.45	77.37	2.05	1.98	2.87
TOTAL LENTICULAR	**104**	**27.96**	**20.63**	.	.	.	.	.
RIBBON COARSE	6	1.61	1.19	1.75	82.74	1.44	1.39	2.43
RIBBON MEDIUM	23	6.18	4.56	1.65	80.95	5.64	5.44	8.98
RIBBON FINE	55	14.78	10.91	1.55	79.16	13.79	13.31	20.63
TOTAL RIBBON	**84**	**22.58**	**16.67**	.	.	.	.	.
				.	.	.	.	.
TOTAL BINDER	**372**	**100.00**	**73.81**	.	.	.	.	.
				.	.	.	.	.
FUSINITE	13		2.58	.	.	.	.	.
SEMI-FUSINITE	34		6.75	.	.	.	.	.
UNIDENTIFIED INERTS	64		12.70	.	.	.	.	.
ALTERED VITRINITE	0		0.00	.	.	.	.	.
GREEN COKE	0		0.00	.	.	.	.	.
DULL COKE	0		0.00	.	.	.	.	.
COAL	0		0.00	.	.	.	.	.
DEPOSITIONAL CARBON	0	0	0.00	.	.	.	.	.
PETROLEUM COKE	0		0.00	.	.	.	.	.
MINERAL	6		1.19	.	.	.	.	.
BONE	15		2.98	.	.	.	.	.
BREEZE	0		0.00	.	.	.	.	.
TOTAL INERTS	**132**		**26.19**	.	.	.	.	.
NOT INC. DEP CARBON			**26.19**	.	.	.	.	.
SOOTY CARBON	0							
SPHERULITIC CARBON	0							
PYROLYTIC CARBON	0							
TOTAL	**0**							
TOTAL COUNTS	**504**		100.00	.	.	103.57115	100.00	**1.155**
CMSI	**2.797**							
BLEND Ro	**1.155**					199.206		
			LV+MV			71.230	**2.797**	
LV	**23.656**		50.54					
MV	**26.882**							
HV	**49.462**	100						

$$CMSI = \frac{\{(\%Incipient)+2(\%CF+\%CM)+3(\%CC+\%LF+\%LM)+4(\%LC+\%RF)+5(\%RM+\%RC)\}}{(100 - \%Isotropic - \%Total\ Inerts)}$$

Results

CSR and CRI Analysis in Pilot-Scale and Sole-Heated Ovens

The primary objective of this work is to validate and compare the measurement of CSR and CRI of cokes produced in the sole-heated oven to those generated in a pilot-scale oven. To achieve this goal, nineteen (19) coal blends were thus carbonized concurrently in both types of ovens at CanmetENERGY.

As described earlier, the CSR test has repeatability and reproducibility limits of 5 and 7, respectively (ASTM D5341-99(2010). The sole heated oven procedure produces coke for CSR testing that is within these limits for comparing to pilot-scale oven results.

Table 2 compares CSR's determined in the two types of ovens. CSR range of the cokes examined was between 42 and 65. The CSR difference, expressed as a %, between ovens is also listed in this table.

Table 2. Comparison of CSR in Pilot Scale and Sole-Heated Ovens

Pilot Scale Oven	Sole Heated Oven	Difference, %
61.9	62.4	0.8
60.5	60.8	0.5
60.3	63.9	6.0
60.3	61.8	2.5
58.0	54.7	-5.7
65.0	63.2	-2.8
51.3	50.9	-0.8
60.5	61.4	1.5
60.6	61.5	1.5
62.7	61.4	-2.1
59.9	56.7	-5.3
42.8	41.5	-3.0
60.9	60.2	-1.2
50.6	51.8	2.4
60.3	61.7	2.3
57.1	55.6	-2.6
54.5	59.0	8.3
52.1	52.4	0.6
57.9	55.6	-4.0

Avg = -0.06%, SD = 3.6%

Figure 3 shows the linear relationship existing between the CSR obtained for the sole heated oven coke and that for the pilot scale oven coke. As can be seen, the data points are evenly distributed on both sides of the line of best fit, indicating that there is no bias due to the coke preparation method. A strong linear relationship ($r^2 = 0.87$) is observed with a slope of 0.88. This indicates that CSR of the coke samples produced using both methods are very similar.

The scattering observed in the data points arises from the accumulated random error in coal handling, coke preparation and CSR measurement, etc. A more detailed analysis of the difference in CSR measured between the two preparation methods reveals that the average of the difference in CSR among the measurements is -0.06% and the standard deviation is 3.6%. The calculated 95% confidence interval is 1.6%. As shown in this error analysis, the CSR measured using sole-heated coke is within ± 2% of the pilot oven CSR value.

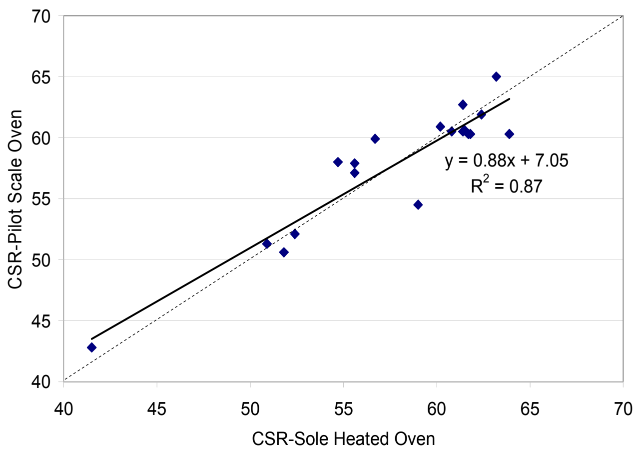

Figure 3. CSR Relationship between Sole-Heated Oven and Pilot Scale Oven

Table 3 compares CRI's measured in the two types of ovens. CRI range of the cokes examined was between 23 and 37. The CRI difference, expressed as a %, between ovens is also listed in this table.

Table 3. Comparison of CRI in Pilot Scale and Sole-Heated Ovens

Pilot Scale Oven	Sole Heated Oven	Difference, %
22.7	23.9	5.3
25.1	25.1	0.0
26.9	24.9	-7.4
25.3	25.0	-1.2
28.1	29.1	3.6
22.5	24.2	7.6
31.0	29.9	-3.5
25.3	25.8	2.0
25.6	26.2	2.3
25.9	25.8	-0.4
26.6	28.0	5.3
35.9	37.2	3.6
26.0	26.9	3.5
32.0	30.8	-3.8
27.6	25.9	-6.2
28.8	30.3	5.2
30.1	27.0	-10.3
31.5	32.8	4.1
26.1	29.0	11.1

Avg = 1.1%, SD = 5.4%

Figure 4 shows the linear relationship existing between the CRI obtained for the pilot scale oven coke and that for the sole-heated oven coke.

As for CSR, there is no apparent bias between the preparation methods on CRI measurement. A strong linear relationship (r^2 = 0.81) is observed with a slope of 0.90 for the line of best fit.

The average of the difference in CRI between the two coke preparation methods is 1.1% and the standard deviation is 5.4%. The calculated 95% confidence interval is 2.4%. Hence, the CRI measured using sole-heated coke is within ± 3% of the pilot oven CRI value.

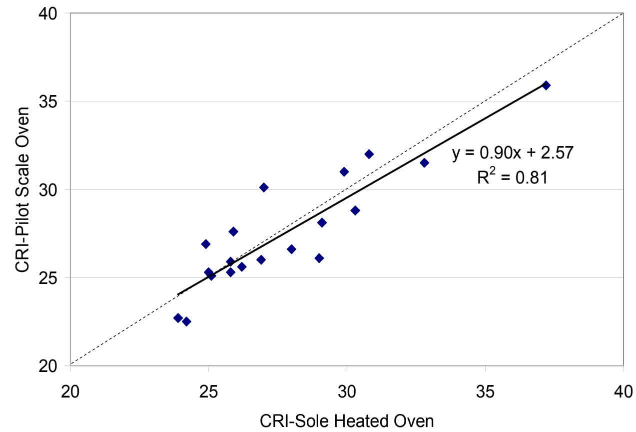

Figure 4. CRI Relationship between Sole-Heated Oven and Pilot Scale Oven

ASG Analysis on Pilot-Scale and Sole-Heated Oven Cokes

To develop a better understanding of the influence of different carbonization methods on the properties of the resulting coke, an analysis of coke ASG was also performed.

As indicated in Table 4, ASG of sole-heated oven cokes are consistently higher than that of pilot oven cokes. In fact for the nineteen (19) cokes examined, ASG of sole-heated oven coke is, on average, about 6% higher than ASG of pilot oven cokes. This finding is mainly attributed to the fact that sole-heated oven cokes are produced under a constant load of 15.2 kPa, which is higher than the pressure exerted on the coal during carbonization in the pilot scale oven, ~8 kPa.

Table 4. Comparison of ASG in Pilot Scale and Sole-Heated Ovens

Pilot Scale Oven	Sole Heated Oven	% Difference
0.935	0.991	6.00%
0.921	0.977	6.11%
0.944	0.994	5.21%
0.921	0.979	6.28%
0.930	0.966	3.88%
0.920	0.967	5.11%
0.918	0.987	7.54%
0.954	1.018	6.70%
0.953	1.001	4.96%
0.953	1.009	5.87%
0.931	0.957	2.81%
0.951	1.016	6.75%
0.930	0.971	4.42%
0.922	0.994	7.89%
0.942	1.012	7.39%
0.956	1.009	5.59%
0.925	0.989	6.95%
0.946	1.002	5.93%
0.927	0.987	6.45%

Avg = 5.9%, SD = 1.3%

Figure 5 shows the linear relationship between ASG measured on sole-heated oven coke and pilot oven coke (slope of 0.56).

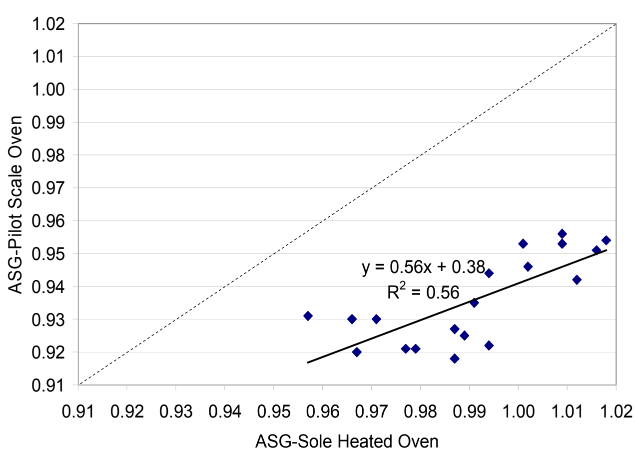

Figure 5. ASG Relationship between Sole-Heated Oven and Pilot Scale Oven

Carbon Form Analysis on Pilot-Scale and Sole-Heated Oven Cokes

Carbon form analysis was performed on seven coke samples from both the pilot-scale movable wall oven (A-G) and the corresponding sole-heated oven (A'-G'). A summary of the carbon form analysis results is given in Table 5. The data in this table shows the total of each category, but for circular, lenticular and ribbon carbon forms (binder phase), each of these contain subcategories based on size of the carbon form itself, i.e., fine, medium and coarse. For isotropic, very fine (incipient) is also included. Inerts (filler phase), are also classified by subgroups such as fusinite, semi-fusinite, and unidentified inerts along with other inerts, which are summed up in the table.

Table 5 shows similar results obtained from both the pilot-scale movable wall oven and the sole heated oven in terms of percent binder phase (reactive) and filler (inert) phase.

Table 5 Carbon Form Analysis Results on Selected Cokes from the Pilot Scale Oven and Sole-Heated Oven

	A	A'	B	B'	C	C'	D	D'	E	E'	F	F'	G	G'
Pilot Scale Oven Test No.	1		2		3		4		5		6		7	
Sole-Heated Oven Test No.		1'		2'		3'		4'		5'		6'		7'
TOTAL ISOTROPIC, %	4.62	2.94	4.78	5.32	5.23	5.20	4.78	4.19	6.36	5.15	4.08	5.07	4.46	2.94
TOTAL CIRCULAR, %	41.30	43.24	32.02	32.41	35.23	35.40	34.27	39.16	26.06	25.57	30.46	26.27	33.86	34.07
TOTAL LENTICULAR, %	21.20	21.76	26.12	25.57	30.23	34.16	15.73	16.01	28.60	29.90	22.54	23.88	21.26	23.04
TOTAL RIBBON, %	14.67	14.12	13.20	15.19	9.77	7.67	12.36	13.79	14.19	13.61	15.59	14.03	13.12	12.01
TOTAL BINDER, %	81.79	82.06	76.12	78.48	80.45	82.43	67.13	73.15	75.21	74.23	72.66	69.25	72.70	72.06
TOTAL FILLER (INERTS), %	18.21	17.94	23.88	21.52	19.55	17.57	32.87	26.85	24.79	25.77	27.34	30.75	27.30	27.94
CMSI	2.77	2.71	2.87	2.84	2.71	2.69	2.73	2.70	2.95	2.90	2.87	2.90	2.80	2.76
BLEND Ro	1.12	1.13	1.15	1.14	1.12	1.12	1.11	1.11	1.17	1.17	1.16	1.16	1.13	1.14
LV, %	19.44	18.64	19.56	19.68	12.71	11.26	18.83	19.87	20.85	20.00	23.43	22.63	19.49	18.20
MV, %	24.42	25.09	32.10	32.26	37.01	39.49	23.01	20.88	36.06	38.61	29.04	32.11	27.80	30.44
HV, %	56.15	56.27	48.34	48.06	50.28	49.25	58.16	59.26	43.10	41.39	47.52	45.26	52.71	51.36

The good relationship between percent binder phase present in sole-heated and pilot scale oven cokes is presented in Figure 6.

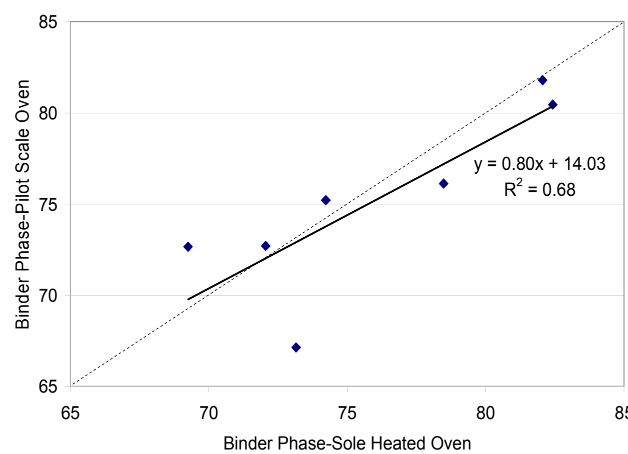

Figure 6. Binder Phase (Reactive) Relationship between Sole-Heated Oven and Pilot Scale Oven Cokes

Also, the sole-heated and pilot scale oven cokes show excellent relationship for 'effective coal blend reflectance, Ro' as presented in Figure 7. This further denotes the similarity of the cokes produced in both types of ovens.

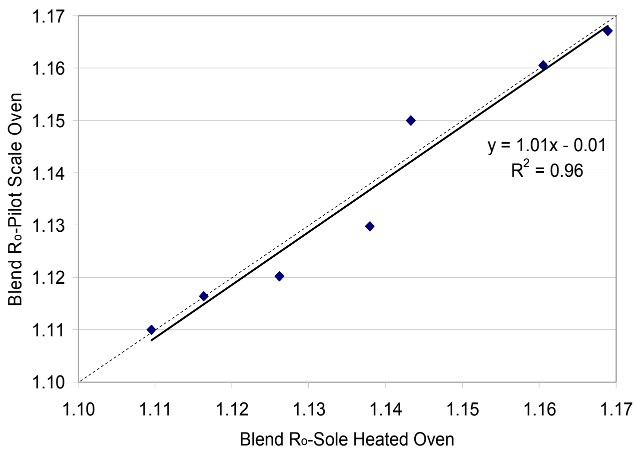

Figure 7. Effective Coal Blend Ro Relationship between Sole-Heated Oven and Pilot Scale Oven Cokes

Applications of Carbon Form Analysis

At ArcelorMittal Dofasco, carbon form analysis is used for many purposes:

- To understand how a given coal will behave during coking.
- To determine the effective rank of a coal based on carbon form analysis.
- To better understand how coal components behave in a blend.
- To clarify caking properties of a coal and or blend.
- To determine coal component blend percentages.
- To determine the amount of inerts in the coke.
- To understand movable wall oven results including pressure generation and coke quality results.
- To clarify coal aging issues that may arise with coal storage.
- To investigate possible contamination issues.
- To understand coal and cokemaking issues for coke production.

Carbon form analysis will lead to a much better understanding of the coals being used or their potential to be used and in what blend scenarios.

To be able to perform carbon form analysis, a coke sample is required. To obtain such a sample, ArcelorMittal Dofasco would normally consider coking a coal or coal blend in a movable wall oven. However, there is a definite need to better understand a coal's behavior during coking before designing these more expensive movable wall oven tests. At ArcelorMittal Dofasco, the coal under investigation is coked in the sole-heated oven using the procedure outlined in this paper. This provides an expansion/contraction value, a coke sample for CSR evaluation from which a sample for carbon form analysis is obtained. Knowing the effective coking ability of the coal and the effective rank of this coal when coke is produced allows determination of how to actually blend this coal.

Knowledge of the coal chemistry, rheology and petrography data does not indicate how the coal itself will behave during cokemaking at the start of our evaluation. Although the coke CSR for a given coal or blend can be potentially predicted, the sole-heated oven technique allows a direct measure of the CSR from the coke produced. If a CSR is poor, a given coal may be rejected before embarking on the more expensive movable wall oven tests.

With respect to coke quality evaluations, this technique has also been used to investigate how a coal can change over time due to stockpiling, including the possible occurrence of aging and contamination. By carbonizing the coal and producing a coke sample for both CSR and carbon form analysis, it is possible to determine if there are coal or cokemaking issues that need to be identified to solve any of these potential issues. Sometimes, the fraction of a specific coal component can be changed or even be removed from the blend.

Another key use for this method is in the coal mining industry. In work related to the characterization of a given coal seam or combination of seams or products from mine exploration projects, this novel technique allows one to actually determine the CSR, the effective rank and coking capability of these samples as the product coke is similar to that produced in a movable wall oven. This is a low cost approach to get real and meaningful data instead of using predictive techniques or only relying on other measurements such as FSI, which could potentially be misleading.

Conclusions

This paper describes the development of a novel procedure at CanmetENERGY for the evaluation of coke CSR using a small-scale carbonization oven – the sole-heated oven.

A comparison between cokes produced in a sole-heated oven using the method developed in this work and those formed in a pilot-scale coke oven found the following:

1. CSR's and CRI's determined are very similar.

2. ASG's for sole-heated oven cokes are higher on account of the higher pressure (load) applied on the coal bed.

3. Carbon forms expressed as binder phase (reactive) and filler phase (inert) are similar.

4. This procedure finds useful applications as a preliminary evaluation method and a reliable screening tool in both the cokemaking and coal mining industry as it provides relevant information on (i) Coking potential/ability of coal/coal blends (ii) CSR evaluation (iii) Carbon form development prior to designing and running pilot oven trials.

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